



## Article

# Capability of Digital Twins for Representing a Complex Process—Prediction of Multicomponent Adsorption Breakthrough Curves and Times

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Received: 29 January 2025 Abstract: This work tries to elucidate the reliability of artificial neural networks Revised: 3 March 2025 (ANN) to predict complex processes. This way, breakthrough curves and Accepted: 4 March 2025 breakthrough times corresponding to 243 different scenarios of the multicomponent Published: 6 March 2025 adsorption of  $H_2$ , CO and CO<sub>2</sub> in a fixed bed from a large set of runs (rather than a single run, which is the majority situation reported in the literature) generated through Aspen Adsorption<sup>TM</sup>, were fitted to 600 ANNs configurations through a homemade software running in Fortran and 8 additional algorithms contained in the Scikit-Learn, a Python module for machine learning. To generate a consistent ANN, data obtained through Aspen Adsorption<sup>TM</sup> were randomly divided into two groups: training (80% of the breakthrough curves and breakthrough times) and validation (20% of them). This procedure was able to properly predict single breakthrough curves. However, the capacity of the ANN for predicting a set of breakthrough curves was not so good as expected although the trends followed by the prediction curves could be used to make a good estimation of the dynamic behaviour of adsorption process. Finally, it was observed a good agreement between the values of the breakthrough times corresponding to the reduction of the H<sub>2</sub> concentration in the outlet stream of 2% computed by Aspen Adsorption<sup>TM</sup> and used for validation and those predicted by the best ANN model. The general procedure here followed could be equally used for analyzing real set of adsorption experiments or other different complex processes as described here.

Keywords: digital twin; multicomponent adsorption; Aspen Adsorption<sup>TM</sup>

## 1. Introduction

Computational tools based on artificial neural networks (ANNs), which are nonlinear regression algorithms in the Machine Learning field for classification and prediction [1], have been successfully used by both academia and industry, and their use is common in Artificial Intelligence (AI). From them, it is possible to obtain a digital twin (DT), which is a virtual model created to represent processes, which can in turn be updated and maintained in real time. AI has introduced new possibilities for modeling and simulating chemical processes [2]. Industry 4.0 requires this piece of knowledge from chemical and process engineers since process plants have large volumes of



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stored historical data obtained through sensors that measure thousands of variables in the order of seconds [3]. Chemical engineers use ANNs in process prediction and classification when there is a lack of both physical understanding of the problem and statistical variations of the observable data [3].

Modeling, simulation, and optimization are essential activities among researchers to meet the challenges produced by environmental and commercial restrictions. In a recent paper [4], DTs based on ANNs were generated for predicting the steady state of styrene production from benzene. The data used were produced from Aspen HYSYS, which led to determining the operating conditions of pre-heating, reaction, and stabilization units. In another recent paper [5], a DT was used to obtain a virtual representation of the experimental data from an alkaline leaching process of black masses from spent batteries. For this purpose, 90% of the experimental data were used for training a supervised learning procedure involving 600 different artificial neural networks (ANNs) derived from twelve different activation functions.

A neural network contains hyperparameters to be tuned prior to training in order to achieve the best configuration. Particularly, activation functions determine the output of the model, its accuracy, and the computational efficiency of training a model; therefore, they are an essential part of the structure of neural networks. The Sigmoid function, Hyperbolic Tangent (TanH), and ReLU (Rectified Linear Unit) are the most common in Chemical Engineering, although many more have been defined [1]. A remarkable challenge is to find the best configuration of layers and activation functions that fit the data of a process.

Another important issue is to know the capability of the ANNs to predict the behaviour of a process when many independent and dependent variables are involved. In this context, the dynamics of adsorption in a fixed bed has been used for dilucidating the capability of the ANNS to describe a complex process. As observed in the literature, most of the studies are focused on the prediction of both the capacity of adsorption and the breakthrough times. Some of them are focused on the prediction of the adsorption dynamic (breakthrough curves) but consider single experiments rather than a set of experiments as proposed here.

The breakthrough time is an important factor in Pressure Swing Adsorption (PSA) cycle design and depends on the adsorption capacity at given conditions, such as temperature, composition, pressure and so on. Specifically, the breakthrough time of hydrogen is a key factor in determining the performance of PSA [6], which is a common method to obtain high-purity hydrogen. The breakthrough time can well reflect the adsorption dynamics and help PSA cycle design. In order to avoid time-consuming and labor-intensive breakthrough curve experiments, it is necessary to develop a fast and accurate surrogate model [6]. ANNs are a good candidate as demonstrated more than 20 years ago [7]. Thus, some studies have been reported for obtaining ANN-based surrogate models that are able to efficiently compute the transient adsorption behavior and breakthrough times without altering the capability of first-principles models [8].

Despite these efforts, challenges remain in studying multicomponent breakthrough curves for hydrogen purification. ANNs and interior point algorithms have been used to optimize the breakthrough time of individual gases in a three-component gas  $H_2/CO/CH_4$  system [9]. This method can only ensure that the breakthrough time of CO or CH<sub>4</sub> is maximum but cannot guarantee that the breakthrough time of both CO and CH<sub>4</sub> can be maximized simultaneously.

ANNs were also applied to model the sorption of dyes blue No. 1 and red No. 2 in aqueous solutions using magnesium and aluminum double layer hydroxides (LDH) interspersed with nitrate ions [10]. Single experimental breakthrough curves were compared with data obtained in the ANN modeling, using four inputs and one output variable for each dye showing an excellent correlation ( $r^2 = 0.99$ ). Three machine learning models (random forest, support vector machine, and artificial neural network) were developed to predict the adsorption capacity of microplastics [11]. The ANN model has been widely used to predict pollutant adsorption in fixed beds under different operating parameters in the treatment of pollutants [12–15]. Modified biochar was used in the adsorption performance of sulfamethoxazole [16]. Based on batch experiment results, an artificial neural network (ANN) model was developed to describe the adsorption data of this pollutant sufficiently ( $r^2 > 0.99$ ). Also, ANNs have been used to describe the adsorption of Cr(VI) from aqueous solutions using activated carbon produced from waste tires [17]. The conjugate gradient backpropagation algorithm was found to be the best training one among all the training algorithms, with a root mean squared error (RSME) of 5.894 and an  $r^2$  of 0.985. The dynamic of the tetracycline adsorption process using raw rice husk was also modeled using ANNs with a correlation coefficient of 0.999 [18].

In a review reported recently, the use of ANNs for evaluating isothermal, kinetic, and thermodynamic parameters in multicomponent adsorption on biomaterials was discussed [19]. The cyclohexane and n-hexane adsorption capacity over graphene was analyzed with a neural network, which was able to predict the experimental values with a correlation coefficient of 0.99966 [20]. In other reviews, the modeling of adsorption of organic and inorganic pollutants from water using ANNs [19,21,22] was reported. ANNs were also used to emulate adsorption

and chromatography processes [23]. The proposed approach focuses on learning the underlying governing partial differential equations in the form of a physics-constrained loss function to simulate adsorption processes accurately. The results demonstrated that the purity and recovery calculated from the neural network-based simulations were within 2.5% of the detailed model predictions. A deep learning artificial neural network framework was also used to optimize the adsorption capacity of 3-nitrophenol using carbonaceous material obtained from biomass wastes [24]. An artificial neural network (ANN) model was improved to estimate the efficiency of Cr(III) and Cr(VI) ions adsorption in aqueous solution on natural, acid-activated and base-activated cherry stalks [25]. A modeling study using ANNs was performed in adsorptive removal of Congo Red on activated hazelnut [26], revealing a correlation of 98%. An ANN model was also able to predict with a higher coefficient of determination and lower root mean square error values the adsorption capacity of organic waste-derived carbonbased materials as a function of the. adsorbent synthesis conditions, adsorbent physical characteristics and adsorption experimental conditions [27]. Feature importance using Shapley additive explanations analysis suggested that the adsorption characteristics with 51.4% were the most important in the ANN prediction. Many more studies have been reported that use ANNs for the prediction of adsorption processes: CO<sub>2</sub> adsorption in metal-organic frameworks (MOFs) [28], silicic acid removal in a fixed-bed column using a modified resin [29], fluoride removal efficiency using neutralized activated red mud from aqueous medium in a continuous fixed bed column [30], time allocation of a three-bed adsorption chiller using an ANN [31], competitive adsorption of dyes on Gemini Polymeric nanoarchitecture [32], fixed-bed phenolic compounds adsorption onto activated date palm biochar [33], mercury adsorption by a dendrimer-grafted polyacrylonitrile fiber in fixed-bed column [34], organic pollutants adsorption on activated carbon [35], adsorption of sunset yellow onto neodymium modified ordered mesoporous carbon [36], Cu(II) adsorption from an aqueous solution [37], heavy metals adsorption dynamic on surfactant decorated graphene [14], color adsorption from an industrial textile effluent using modified sugarcane bagasse [38], asphaltenes adsorption by nanocomposites [39], adsorption of methylene blue in a fixed bed column [40], Pb(II) adsorption [41,42], malachite green adsorption by tea waste [43], Cr(VI) adsorption from aqueous solution with Aliquat 336-derived adsorbents [44], Ni(II) adsorption from aqueous solution by peanut shell [45], Sr(II) adsorption from aqueous solution by natural calcium-based materials [46], and adsorption chromatography of chitosanases produced by Paenibacillus ehimensis [47], among others.

On the other hand, Aspen Adsorption<sup>TM</sup>, which is integrated into the AspenTech software, is a very powerful tool for simulating adsorption processes. Aspen Adsorption enables process simulation and optimization for a wide range of industrial gas and liquid adsorption processes, including reactive adsorption, ion exchange, and cyclic processes. Despite that few studies are using Aspen Adsorption<sup>TM</sup> as a tool for simulating adsorption processes [48]. Some examples have been reported in the literature: a single bed Pressure Swing Adsorption (PSA) unit for the carbon capture process of CO<sub>2</sub> and H<sub>2</sub> [48], different configuration of adsorption units including pressure swing ones [49], six-step pressure swing adsorption process for biogas separation on a commercial scale [50], etc. In a recent study [51], an ANN was used to optimize a six-step two-bed pressure swing adsorption system for hydrogen purification. The pressure swing adsorption model used for describing the hydrogen purification was developed on the Aspen/Adsorption software platform.

This work tries to elucidate the reliability of ANNs to predict a complex process. Thus, the dynamics of a set of experiments of adsorption in a fixed bed were considered. As mentioned above, this study faces the capability of the ANNs to predict both the breakthrough curves and the breakthrough times of multicomponent adsorption in a fixed bed from a large set of runs (rather than a single run, which is the majority situation reported in the literature) generated through Aspen Adsorption<sup>TM</sup>. The system considered was constituted by a stream containing  $H_2$ , CO and CO<sub>2</sub>. Basic data for performing the simulation was taken and adapted from the literature [52]. The adsorbent used was a mixture with the same amount by weight of zeolite and activated carbon. From that, 243 different scenarios were generated with the software mentioned above. From them, it was selected sets of data depending of the ending time of the simulation: 25, 50, 100 and 200 s. The different sets were fitted to 600 ANNs configurations through homemade software running in Fortran. Eight additional algorithms contained in the Scikit-Learn, a Python module for machine learning: Linear regression, Ridge, Lasso, Lars, LassoLars, MultiTaskElasticNet, and OrthogonalMatchingPursuit, were also considered. An MS Escel-VBA application was built to control the data transfer from this application to the Fortran and Python ones. Data collected were compared and the best results were selected. Regarding the input variables, seven were considered in this study: time on stream, compositions in molar fraction of methane, carbon monoxide and hydrogen, and pressure at the inlet stream to the process and the height and diameter of the bed. Three output variables were considered: molar fractions of methane, carbon monoxide and hydrogen at the effluent stream of the process. To generate a consistent ANN, the data obtained through Aspen Adsorption<sup>TM</sup> was randomly divided into two groups: (i) 80% of the breakthrough

curves and breakthrough times, which were used for ANNs training, and (ii) 20% of them, which were used for validation.

# 2. Materials and Methods

# 2.1. Aspen Adsorption<sup>TM</sup>

Aspen Adsorption<sup>TM</sup> was used for generating the 243 scenarios mentioned above. Before running a scenario, a set of steps should be followed (Figures S1–S5): fluid package definition (Peng-Robinson) and components selection (CH<sub>4</sub>, CO and H<sub>2</sub>), simulation mode definition (in this case "Gas Dynamic"), blocks selection (the main one is "Gas Bed"), and configuration of the geometric properties of the bed and its layers. Figure 1 shows the final flowsheet used in the simulation.



**Figure 1.** Flowsheet used for the simulation of a fixed bed with Aspen Adsorption<sup>TM</sup>. Data of the seven input variables and the three output variables were recorded each second of the simulation run.

# 2.2. ANNs

In a previous work [5], the procedure for training and validating models here followed is described, which is more extensively explained in the Supplementary Materials section. Apart from the seven activation functions listed in Table 1 [4,53–57], additional models taken from the Python module for machine learning Scikit-Learn (https://scikit-learn.org/stable/, accessed on 15 January 2025): Linear regression, Ridge, Lasso, Lars, LassoLars, MultiTaskElasticNet, and OrthogonalMatchingPursuit, were also considered. In the input layer, the number of input variables (independent variables) fixed the number of neurons of the layer, whereas in the output layer, the numbers of neurons were fixed by the number of output variables (dependent variables). One or two hidden layers were considered. In this way, the neural network learning capacity was determined by the number of hidden layers as well as the neurons contained in each layer. By combining the seven activation functions listed in Table 1 and considering 2 or 3 layers, 600 different configurations could be defined. An MS Excel-VBA application (register number TXu 2-443-000 of the Copyright Office of USA) was built to control the data transfer from this application to other two (system model): an executable file generated from a Fortran code which sped up the numerical computations of the 600 models derived from Table 1, and an script written in Python to run the 8 models included in the Scikit-Learn module. The MS Excel-VBA collected the results generated by these two applications and performed the fitting and validation processes of all the models considered here. Adding up the functions considered from Scikit-Learn, the total number of models tested was 608. Seven input variables were considered in this study: time on stream, compositions in molar fraction of methane, carbon monoxide and hydrogen, and pressure at the inlet stream to the process and the height and diameter of the bed. Three output variables were considered: molar fractions of methane, carbon monoxide and hydrogen at the effluent stream of the process.

| <b>Activation Function</b> | ID Code | Mathematical Expression   |
|----------------------------|---------|---|
| Log-Sigmoid                | LOGSIG  | $a_j = \frac{1}{1 + e^{-n_j}}$  |
| Hyperbolic Tangent Sigmoid | HTANSIG | $a_j = \frac{e^{n_j} - e^{-n_j}}{e^{n_j} + e^{-n_j}}$                       |
| Linear                     | LINEAR  | $a_j = n_j$   |
| Swish                      | SWISH   | $a_j = \frac{n_j}{1 + e^{-n_j}}$  |
| ELU                        | ELU     | $a_j = egin{cases} lpha(e^{n_j}-1) & n_j < 0 \ n_j & n_j \ge 0 \end{cases}$ |
| RELU                       | RELU    | $a_j = egin{cases} 0.01 n_j & n_j \leq 0 \ n_j & n_j > 0 \end{cases}$       |
| Polynomial *               | POL     | $a_j = n_j^i$   |

Table 1. Activation functions used in this study for generating ANNs [4,53–57].

\* where *i* is in the range from 1 to the total neurons in layer *j*.

The training process was performed by minimizing the function  $\chi_j^2$  by nonlinear regression by using the Levenberg-Marquardt algorithm [58]:

$$\chi_j^2 = \sum_{i=1}^m \left[ \sum_{k=1}^n (y_{ik} - a_{ikj}^s)^2 \right]$$
(1)

where *m* is the number of experiments, *n* is the number of output variables,  $y_{ik}$  and  $a_{ikj}^s$  are the values of the output experimental variables and the values predicted by the neural network that corresponds to scenario *j*, respectively.

The regression procedure was maintained whenever the relative error (*RE*) was lower than  $10^{-4}$ . The *RE* was defined as follows:

$$RE = \left| \frac{(x_k^2)_{j+1} - (x_k^2)_j}{(x_k^2)_j} \right|$$
(2)

being *j* the number of iterations in the non-linear regression procedure, comparing the results of the prediction made by the ANN in the scenario j and the scenario j + 1.

Once the fitting process for a given scenario is finished, the above-defined function  $\chi_j^2$ , the Pearson's ratio coefficient for the model, *r*, and the root mean squared error (*RSME*) were collected. The *RMSE* was defined as:

1

$$RMSE_j = \sqrt{\frac{\chi_j^2}{M}}$$
(3)

To minimize overfitting in the validation process, a discrimination procedure was established. For this purpose, a function presented by Equation (1) was defined for the experiments used for the validation  $(m_V)$ , obtaining Equation (4):

$$\left(\chi_{j}^{2}\right)_{V} = \sum_{i=1}^{m_{V}} \left[ \sum_{k=1}^{n} \left( y_{ik} - a_{ikj}^{s} \right)^{2} \right]$$
(4)

This way, a new function was defined from Equations (1) and (4):

$$\left(\chi_j^2\right)_{\mathrm{T}} = \chi_j^2 + \left(\chi_j^2\right)_{\mathrm{V}} \tag{5}$$

Finally, a non-linear regression was performed with the selected model until a new value of *RE* lower than  $10^{-6}$  was reached. With the values of the parameters finally obtained, the validation procedure was completed. In both cases, the final fitting and validation, the above defined function  $\chi_j^2$  plus those defined for each output variable *k*, can be expressed as  $\chi_{ik}^2$ :

$$\chi_{jk}^2 = \sum_{i=1}^m (y_{ik} - a_{ikj}^s)^2 \tag{6}$$

To generate a consistent ANN, the data obtained through Aspen Adsorption<sup>TM</sup> was randomly divided into two groups: (i) 80% of the breakthrough curves were used for ANNs training, and (ii) 20% of them were used for validation.

The MS Excel-VBA application described above was able to compute the Pearson's ratio coefficient for the model, *r*, the Shapley values through the Kernel SHAP approximation [59], and the dimensionless sensitivity values derived from the partial derivatives method [60]. In this study, the latter was used for comparative purposes. Figure 2 shows a schematic representation of the computational procedure described above.



Figure 2. Block diagram of the numerical procedure followed for selecting the best model for representing breakthrough curves.

An important issue of this fitting process is the time required to fit the huge number of data. Taking as a reference the set of data corresponding to a time on stream of 200 s, about 50,000 data consisting of seven independent variables and three dependent ones were fitted to the 608 models in a time lower than 3 h using a computer with an Intel Core i7-12700K processor. This time included the discrimination and validation processes.

The results listed in Tables 2–4 and Table S1 include a nomenclature to identify a particular ANN. For example, 7-SWISH-3-HTANSIG-4-LINEAR-3 represents a ANN with three layer of neurons: the first one receives the 7 input variables and contains 3 neurons with a Swish activation function, the second one receives the 3 inputs from the first one and contains 4 neurons with a Hyperbolic Tangent Sigmoid activation function; and, the third one receives 4 inputs from the second one and contains 3 neurons (coincidental with the number of output variables of the system: molar fractions of the three species involved) with a Linear activation function. Figure 3 shows as an example the representation of the 7-SWISH-3-HTANSIG-4-LINEAR-3 artificial neural network.

**Table 2.** The best five ANN models that fitted a breakthrough curve obtained with Aspen Adsorption<sup>TM</sup> for the following input variables: bed height, 1 m; bed diameter, 0.015 m; pressure, 2000 kPa; molar fractions of CH<sub>4</sub>, CO and H<sub>2</sub>, 0.35, 0.14, 0.51, respectively.

| Order | Model                     | RMSE                   | $(r^2)_{\text{training}}$ | (χ <sup>2</sup> )τ     |
|-------|---------------------------|------------------------|---------------------------|------------------------|
| 1     | 7-RELU-4-SWISH-4-LINEAR-3 | $1.474 \times 10^{-2}$ | 0.988                     | $4.365 \times 10^{-2}$ |
| 2     | 7-RELU-4-SWISH-5-LINEAR-3 | $1.483 \times 10^{-2}$ | 0.987                     | $4.421 \times 10^{-2}$ |
| 3     | 7-ELU-5-POL-5-LINEAR-3    | $1.987 \times 10^{-2}$ | 0.977                     | $7.936 \times 10^{-2}$ |
| 4     | 7-RELU-4-RELU-2-LINEAR-3  | $2.018 \times 10^{-2}$ | 0.977                     | $8.184 \times 10^{-2}$ |
| 5     | 7-RELU-2-ELU-4-LINEAR-3   | $2.025 	imes 10^{-2}$  | 0.976                     | $8.214 	imes 10^{-2}$  |

**Table 3.** Best ANN models that fitted the data obtained with each of the time on stream. Number of breakthrough curves for training: 194. Number of breakthrough curves for validation: 49.

|   | Time on stre   | eam = 25 s                |                    |                             |
|---|--|---------------------------|--------------------|-----------------------------|
| Number of data for tr   | Number of data for training = 5044. Number of data for validation = $1274$ |                           |                    |                             |
| Model   | RMSE   | $(r^2)_{\text{training}}$ | $(\chi^2)_{\rm T}$ | $(r^2)_{\text{validation}}$ |
| 7-RELU-3- HTANSIG-3-LINEAR-3  | $1.556 \times 10^{-2}$   | 0.986                     | 1.487              | 0.903                       |
| Time on stream = $50 \text{ s}$   |  |                           |                    |                             |
| Number of data for training = $9894$ . Number of data for validation = $2499$ |  |                           |                    |                             |

| Model                       | RMSE                   | $(r^2)_{\text{training}}$ | $(\chi^2)_{\rm T}$    | $(r^2)_{\text{validation}}$ |
|-----------------------------|------------------------|---------------------------|-----------------------|-----------------------------|
| 7-SWISH-3-POL-3-LINEAR-3    | $5.303 \times 10^{-2}$ | 0.916                     | 3.646 × 10            | 0.903                       |
|                             | Time on stre           | am = 100 s                |                       |                             |
| Number of data for tr       | aining = 19,594.       | Number of data f          | For validation = 4949 |                             |
| Model                       | RMSE                   | $(r^2)_{\text{training}}$ | $(\chi^2)_{\rm T}$    | $(r^2)$ validation          |
| 7-ELU-5-LINEAR-3            | $2.311 \times 10^{-2}$ | 0.990                     | $1.363 \times 10$     | 0.987                       |
|                             | Time on stre           | am = 200 s                |                       |                             |
| Number of data for t        | aining = 38,994.1      | Number of data f          | or validation = 9849  |                             |
| Model                       | RMSE                   | $(r^2)_{\text{training}}$ | $(\chi^2)_{\rm T}$    | $(r^2)_{\text{validation}}$ |
| 7-RELU-2-HTANSIG-4-LINEAR-3 | $7.339 \times 10^{-2}$ | 0.906                     | $2.629 \times 10^{2}$ | 0.907                       |

**Table 4.** Relative importance in percentage for each set of times on stream data of the independent variables (inputs) in each dependent variable (outputs) evaluated by the partial derivates method [60].

|                                 | Time on St                     | ream = 25 s                                     |                                   |
|---------------------------------|--------------------------------|---|-----------------------------------|
|                                 |                                | Outputs   |                                   |
| Inputs                          | $(\mathcal{Y}_{CH4})_{outlet}$ | $(\mathcal{Y}_{\mathrm{CO}})_{\mathrm{outlet}}$ | $(y_{H2})_{outtlet}$              |
| Time (s)                        | 43.16 (+)                      | 43.16 (+)                                       | 43.16 (-)                         |
| Height of the bed (m)           | 1.87 (-)                       | 1.87 (-)  | 1.87 (+)                          |
| Bed diameter (m)                | 0.10 (-)                       | 0.10 (-)  | 0.10 (+)                          |
| Pressure (kPa)                  | 54.39 (+)                      | 54.39 (+)                                       | 54.39 (-)                         |
| $(\gamma_{CH4})_{inlet}$        | 0.27 (+)                       | 0.27 (+)  | 0.27 (-)                          |
| $(\gamma_{\rm CO})_{\rm inlet}$ | 0.04 (+)                       | 0.04 (+)  | 0.04 (-)                          |
| (VH2)inlet                      | 0.17 (+)                       | 0.17 (+)  | 0.17 (-)                          |
|                                 | Time on St                     | ream = 50 s                                     |                                   |
|                                 |                                | Outputs   |                                   |
| Inputs                          | (VCH4)outlet                   | $(\gamma_{\rm CO})_{\rm outlet}$                | $(\gamma_{\rm H2})_{\rm outtlet}$ |
| Time (s)                        | 62.52 (+)                      | 53.72 (+)                                       | 60.97 (-)                         |
| Height of the bed (m)           | 1.56 (-)                       | 2.30 (-)  | 1.69 (+)                          |
| Bed diameter (m)                | 0.10 (-)                       | 0.06 (-)  | 0.09 (+)                          |
| Pressure (kPa)                  | 29.26 (+)                      | 36.29 (+)                                       | 30.51 (-)                         |
| $(\mathcal{Y}_{CH4})_{inlet}$   | 1.31 (-)                       | 1.74 (-)  | 1.38 (+)                          |
| (VCO)inlet                      | 0.33 (-)                       | 0.29 (-)  | 0.32(+)                           |
| (VH2)inlet                      | 4.92 (-)                       | 5.60 (-)  | 5.04 (+)                          |
|                                 | Time on Str                    | eam = 100 s                                     |                                   |
|                                 |                                | Outputs   |                                   |
| Inputs                          | $(\gamma_{CH4})_{outlet}$      | $(\gamma_{\rm CO})_{\rm outlet}$                | $(y_{H2})_{outtlet}$              |
| Time (s)                        | 73.32 (+)                      | 80.98 (+)                                       | 74.70 (-)                         |
| Height of the bed (m)           | 2.18 (-)                       | 2.51 (-)  | 2.24 (+)                          |
| Bed diameter (m)                | 0.05 (-)                       | 0.06 (-)  | 0.05 (+)                          |
| Pressure (kPa)                  | 23.72 (+)                      | 15.96 (+)                                       | 22.33 (-)                         |
| (VCH4)inlet                     | 0.35 (+)                       | 0.10 (+)  | 0.30 (-)                          |
| $(\gamma_{\rm CO})_{\rm inlet}$ | 0.01 (+)                       | 0.11 (+)  | 0.03 (-)                          |
| $(y_{\rm H2})_{\rm inlet}$      | 0.37 (-)                       | 0.28 (-)  | 0.35 (+)                          |
|                                 | Time on Str                    | eam = 200 s                                     |                                   |
|                                 |                                | Outputs   |                                   |
| Inputs                          | $(\gamma_{CH4})_{outlet}$      | $(\gamma_{\rm CO})_{\rm outlet}$                | $(y_{H2})_{outtlet}$              |
| Time (s)                        | 77.39 (+)                      | 76.49 (+)                                       | 77.21 (-)                         |
| Height of the bed (m)           | 4.30 (-)                       | 4.68 (-)  | 4.38 (+)                          |
| Bed diameter (m)                | 0.24 (-)                       | 0.21 (-)  | 0.23 (+)                          |
| Pressure (kPa)                  | 16.85 (+)                      | 18.09 (+)                                       | 17.10 (-)                         |
| (VCH4)inlet                     | 0.52 (+)                       | 0.36 (+)  | 0.48 (-)                          |
| (VCO)inlet                      | 0.03 (+)                       | 0.04 (+)  | 0.04 (-)                          |
| (VH2)inlet                      | 0.67(-)                        | 0.13(-)   | 0.56(+)                           |

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Figure 3. Representation of the 7-SWISH-3-HTANSIG-4-LINEAR-3 artificial neural network.

# 3. Results

As above mentioned, 243 scenarios were generated with Aspen Adsorption<sup>TM</sup> by using data taken and adapted from literature [53]. The adsorbent considered was a mixture with the same amount by weight of zeolite and activated carbon. Figure 4 shows the general physical parameters used by Aspen Adsorption<sup>TM</sup>. Table 5 lists the properties of the inlet stream to the process (Feed in Figure 1) whereas Table 6 does the values of the parameters used for generating all the scenarios.

| BED.Layer(1).Specify Ta | ble        |                 |                                      |
|-------------------------|------------|-----------------|--------------------------------------|
|                         | Value      | Units           | Description                          |
| Hb                      | 1,0        | m               | Height of adsorbent layer            |
| Db                      | 0,037      | m               | Internal diameter of adsorbent layer |
| Ei                      | 0,433      | m3 void/m3 bed  | Inter-particle voidage               |
| Ep                      | 0,347      | m3 void/m3 bead | Intra-particle voidage               |
| RHOs                    | 850,0      | kg/m3           | Bulk solid density of adsorbent      |
| Rp                      | 0,0015     | m               | Adsorbent particle radius            |
| SFac                    | 1,0        | n/a             | Adsorbent shape factor               |
| MTC(*)                  |            |                 |                                      |
| MTC("CH4")              | 0,195      | 1/s             | Constant mass transfer coefficients  |
| MTC("CO")               | 0,15       | 1/s             | Constant mass transfer coefficients  |
| MTC("H2")               | 0,7        | 1/s             | Constant mass transfer coefficients  |
| IP(*)                   |            |                 |                                      |
| IP(1,"CH4")             | 0,02386    | n/a             | Isotherm parameter                   |
| IP(1,"CO")              | 0,03385    | n/a             | Isotherm parameter                   |
| IP(1,"H2")              | 0,01694    | n/a             | Isotherm parameter                   |
| IP(2,"CH4")             | 5,621e-005 | n/a             | Isotherm parameter                   |
| IP(2,"CO")              | 7,2e-007   | n/a             | Isotherm parameter                   |
| IP(2,"H2")              | 2,1e-005   | n/a             | Isotherm parameter                   |
| IP(3,"CH4")             | 0,003478   | n/a             | Isotherm parameter                   |
| IP(3,"CO")              | 2,311e-004 | n/a             | Isotherm parameter                   |
| IP(3,"H2")              | 6,248e-005 | n/a             | Isotherm parameter                   |
| IP(4,"CH4")             | 1159,0     | n/a             | Isotherm parameter                   |
| IP(4,"CO")              | 1751,0     | n/a             | Isotherm parameter                   |
| IP(4,"H2")              | 1229,0     | n/a             | Isotherm parameter                   |
|                         | •          |                 |                                      |

Figure 4. Physical properties of the fixed bed used as the reference.

| Table 5. Properties | of the inlet stream | to the process | (Feed in | Figure 1) |
|---------------------|---------------------|----------------|----------|-----------|
| 1                   |                     | 1              |          | 0 ,       |

| Variable               | Value  |  |
|------------------------|--------|--|
| Molar Flowrate (mol/s) | 5      |  |
| Temperature (K)        | 298.15 |  |
| Pressure (kPa)         | 980    |  |
| Усн4                   | 0.281  |  |
| усо                    | 0.115  |  |
| Ун2                    | 0.604  |  |

**Table 6.** Values of the parameters used for generating all the scenarios analyzed (243). The temperature and the molar flowrate were fixed at 298.15 K and 5 mol/s, respectively. Pressures and molar fractions are those of the inlet stream.

| Variable              |                        | Values                 |                        |
|-----------------------|------------------------|------------------------|------------------------|
| Pressure (kPa)        | 900                    | 1480                   | 2000                   |
| Height of the bed (m) | 0.5                    | 1                      | 2                      |
| Bed diameter (m)      | 0.015                  | 0.037                  | 0.050                  |
| (VCH4)inlet           | 0.25                   | 0.30                   | 0.35                   |
| (VCO) inlet           | 0.08                   | 0.11                   | 0.14                   |
| (VH2)inlet            | $1 - y_{CH4} - y_{CO}$ | $1 - y_{CH4} - y_{CO}$ | $1 - y_{CH4} - y_{CO}$ |

By modifying the final time of the simulation, the number of data generated in each case was different. As mentioned above, data of the 243 scenarios were recorded each second of the simulation run, 80% of the breakthrough curves being used for ANNs training, whereas 20% of them being used for validation. Thus, for a value of this variable of 25 s, the number of data collected was 6318; for a value of 50 s, the number of data was 12,393, for a value of 100 s, the number of data was 24,543; and for a value of 200 s, the number of data was 48,843.

## 4. Discussion

Figure 5 shows the breakthrough curve generated by Aspen Adsorption<sup>TM</sup> for a time on stream of 600 s taken as a reference to the inlet conditions listed in Table 5. It can be seen that the steady state values for the molar fractions of CH<sub>4</sub>, CO and H<sub>2</sub> in the effluent coming from the process were mostly attained at a time on stream lower than 200 s. Similar trends were observed for the rest of the runs. This time was considered the higher value for the analysis performed in this work.



**Figure 5.** Evolution of the molar fractions of  $CH_4$ , CO and  $H_2$  in the effluent for a time on stream of 600 s. The conditions of the inlet stream are listed in Table 2. Image taken from Aspen Adsortpion<sup>TM</sup>.

First of all, it was checked that the procedure raised was able to work for a single breakthrough curve. As shown in Figure 6, it was found a model (7-RELU-4-SWISH-4-LINEAR-3) that fitted it well, demonstrating the capability of the procedure followed for predicting single breakthrough curves. Table 2 lists the five best ANN models that fitted the data obtained from the simulation performed by Aspen Adsorption<sup>TM</sup>. Similar results were obtained when other single breakthrough curves were fitted.



**Figure 6.** Breakthrough curve obtained with Aspen Adsorption<sup>TM</sup> for CH<sub>4</sub>, CO and H<sub>2</sub> and predicted results for a single breakthrough curve. Input variables: bed height, 1 m; bed diameter, 0.015 m; pressure, 2000 kPa; molar fractions of CH<sub>4</sub>, CO and H<sub>2</sub>, 0.35, 0.14, 0.51, respectively.

Then, 80% of the breakthrough curves data for times on stream of 25, 50, 100, and 200 s were fitted to the 608 ANN models selected in this work. Table 3 shows the best ANN models that fitted the data obtained with each

of the time on stream considered. Table S1 lists, as an example, the five best models for a time on stream of 100 s. It can be observed that different best ANN models were selected as a function of the time on stream considered. In general, the determination coefficient is in some cases as high as those obtained for a single breakthrough curve. However, the values of this coefficient for the validation process for all the times on stream considered were lower. Figures 7–9 show for some runs used for validation the quality of prediction reached with the best models considered for each time on stream. As checked, the capacity of the ANN for predicting breakthrough curves is not as good as expected, although the trends followed by the prediction curves could be used to make a good estimation of the dynamic behaviour of the adsorption process.



**Figure 7.** Breakthrough curves obtained with Aspen Adsorption<sup>TM</sup> for CH<sub>4</sub>, CO and H<sub>2</sub> and predicted results at times on stream of 25, 50, 100 and 200 s. Input variables: bed height, 1 m; bed diameter, 0.037 m; pressure, 900 kPa; molar fractions of CH<sub>4</sub>, CO and H<sub>2</sub>, 0.30, 0.14, 0.56, respectively. This run was in the pack of runs used for validation.



**Figure 8.** Breakthrough curves obtained with Aspen Adsorption<sup>TM</sup> for CH<sub>4</sub>, CO and H<sub>2</sub> and predicted results at times on stream of 25, 50, 100 and 200 s. Input variables: bed height, 1 m; bed diameter, 0.037 m; pressure, 2000 kPa; molar fractions of CH<sub>4</sub>, CO and H<sub>2</sub>, 0.25, 0.14, 0.61, respectively. This run was in the pack of runs used for validation.



**Figure 9.** Breakthrough curves obtained with Aspen Adsorption<sup>TM</sup> for CH<sub>4</sub>, CO and H<sub>2</sub> and predicted results at times on stream of 25, 50, 100 and 200 s. Input variables: bed height, 1 m; bed diameter, 0.037 m; pressure, 1480 kPa; molar fractions of CH<sub>4</sub>, CO and H<sub>2</sub>, 0.30, 0.14, 0.56, respectively. This run was in the pack of runs used for validation.

On the other hand, Table 4 shows the relative importance of the independent variables (inputs) in each dependent variable (outputs) evaluated by the partial derivates method [60]. If the positive variation of an independent variable led to a positive variation of a dependent one the sign would be +; in the contrary case, it would be -. It can be observed that the relative importance of each dependent variable for all the sets of experiments considered was mainly a function of the time on stream and the pressure. It was also observed that the sign of some matches of independent and dependent variables was also a function of the set of time on stream considered.

In summary, the results obtained in this study showed that although the ANN models can be used to predict the behaviour of breakthrough curves of multicomponent adsorption processes, the quality of the prediction was not as good as expected when the number of breakthrough curves considered was different from one.

Finally, an ANN model was used to predict the breakthrough times corresponding to the reduction of the  $H_2$  concentration in the outlet stream of 2% for all the scenarios raised. Again, 80% of the values obtained by simulation were used for training, whereas the remaining ones were used for validation. Table 7 shows the best ANN model, whereas Table 8 lists the relative importance of the independent variables (inputs) on the dependent variable (breakthrough time) evaluated by the partial derivates method. Again, the main input variable affecting the breakthrough time was the pressure, the sign being negative. Figure 10 shows a comparison between the values of the breakthrough times computed by Aspen Adsorption<sup>TM</sup> and used for validation and those predicted by the best ANN model. As confirmed by the  $(r^2)_{validation}$  value, a good agreement between both sets of values was reached.

| Table 7. Best ANN model that fitted the breakthrough tin |
|--|
|--|

| Model                  | RMSE                   | (r <sup>2</sup> )training | $(\chi^2)_{\rm T}$    | ( <i>I</i> <sup>2</sup> )validation |
|------------------------|------------------------|---------------------------|-----------------------|-------------------------------------|
| 7-POL-4-ELU-3-LINEAR-1 | $8.319 \times 10^{-1}$ | 0.9998                    | $1.457 \times 10^{2}$ | 0.9998                              |

| Table 8. Relative importance in percentage for each set of times on stream data of the independent variables (input | 5) |
|---|----|
| on the dependent variable (breakthrough time) evaluated by the partial derivates method [60].                       |    |

| Inputs -              | Output            |
|-----------------------|-------------------|
|                       | Breakthrough Time |
| Height of the Bed (m) | 0.37 (+)          |
| Bed Diameter (m)      | 0.00 (0)          |
| P (kPa)               | 99.58 (-)         |
| УСН4                  | 0.00 (0)          |
| Усо                   | 0.00 (0)          |
| УН2                   | 0.00 (0)          |



Figure 10. Comparison between the values of the breakthrough times computed by Aspen Adsorption<sup>TM</sup> and used for validation and those predicted by the best ANN model.

The methodology here presented for the analysis of adsorption processes can be easily extrapolated to other separation or conversion processes and for the computation of thermodynamic properties. Two studies are currently running which take advantage of the experience here acquired: prediction of thermodynamical properties from COnductor-like Screening Model (COSMO) computations and evaluation of the sensitivity of characterization properties of catalysts on their catalytic performance.

#### 5. Conclusions

This work analyzes the reliability of ANNs to predict a complex process. This way, breakthrough curves and breakthrough times of the multicomponent adsorption of H<sub>2</sub>, CO and CO<sub>2</sub> in a fixed bed from a large set of runs (rather than a single run, which is the majority situation reported in the literature) generated through Aspen AdsorptionTM. As an example, a system constituted by a stream containing H<sub>2</sub>, CO and CO<sub>2</sub> was considered. Thus, 243 different scenarios were generated with the software mentioned above. From them, it was selected sets of data depending on the ending time of the simulation: 25, 50, 100 and 200 s. The different sets were fitted to 600 ANNs configurations through a homemade software running in Fortran. Eight additional algorithms contained in the Scikit-Learn, a Python module for machine learning, were also considered. To generate a consistent ANN, the data obtained through Aspen Adsorption<sup>TM</sup> was randomly divided into two groups: (i) 80% of the breakthrough curves and breakthrough times, which were used for ANNs training, and (ii) 20% of them, which were used for validation. After checking that the procedure raised was able to work for a single breakthrough curve, it was observed that the capacity of the ANN for predicting a set of breakthrough curves was not so good as expected although the trends followed by the prediction curves could be used to make a good estimation of the dynamic behaviour of adsorption process. Finally, ANN models were used to predict the breakthrough times corresponding to the reduction of the H<sub>2</sub> concentration in the outlet stream of 2% for all the scenarios raised. A good agreement was observed between the values of the breakthrough times computed by Aspen Adsorption<sup>TM</sup> and used for validation and those predicted by the best ANN model. The general procedure followed here could be equally used for analyzing a real set of adsorption experiments or other different complex processes as described here.

#### **Supplementary Materials**

The additional data and information can be downloaded at: https://www.sciltp.com/journals/acpa/2025/1/725/s1. References [61–64] are cited in the supplementary materials.

#### **Author Contributions**

Conceptualization, J.L.V. and A.G.-F.; methodology, V.R.F. and M.M.R.-D.; software, J.L.V.; data curation, V.R.F. and A.G.-F.; writing—original draft preparation, J.L.V. and V.R.F.; visualization, V.R.F. and M.M.R.-D.; investigation, all; supervision, V.R.F. and J.L.V.; software, validation, J.L.V. and M.M.R.-D.; writing—review and editing, V.R.F. and A.G.-F. All authors have read and agreed to the published version of the manuscript.

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## **Data Availability Statement**

The original contributions presented in the study are included in the article and Supplementary Materials; further inquiries can be directed to the corresponding author.

# **Conflicts of Interest**

The authors declare no conflict of interest.

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